



# Aerospace Combustion

## Lecture 7:

### Short Introduction to Chemical Mechanism Reduction



## Current Status of Mechanism Development

1. Many simple mechanisms exist which are tuned for a small range of boundary conditions and molecules.
2. A mechanism developed for one class/range of phenomena may not be applicable to another class/range of phenomena
3. A mechanism is comprehensive only if it validated against experimental data of all relevant phenomena and parametric ranges
4. Validation is meaningful only if experimental data are accurate/meaningful
5. Presently, no comprehensive detailed mechanisms exist even for simple fuels



## Mechanism Construction

### Species

- Reactants
- Intermediates, Radicals
- Products

### Elementary Reactions

### Physico-chemical Data for all Species

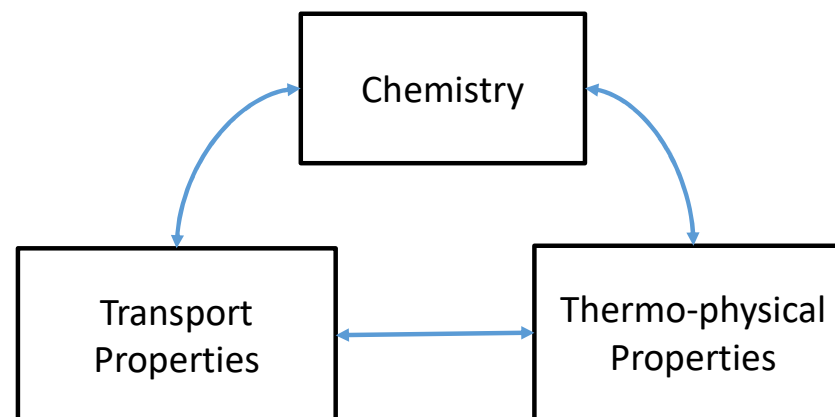
- Enthalpy of Formation
- Entropy
- Heat Capacity
- Transport Properties

### Rate Constants of Reaction

- Phenomenological Arrhenius law

$$k = A \cdot e^{(-E_a/RT)}; \quad k = A \cdot T^n e^{(-E/RT)}$$

- Pressure Dependency



### Transport Properties

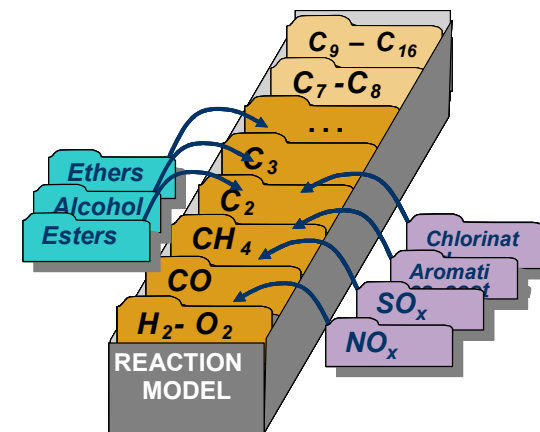
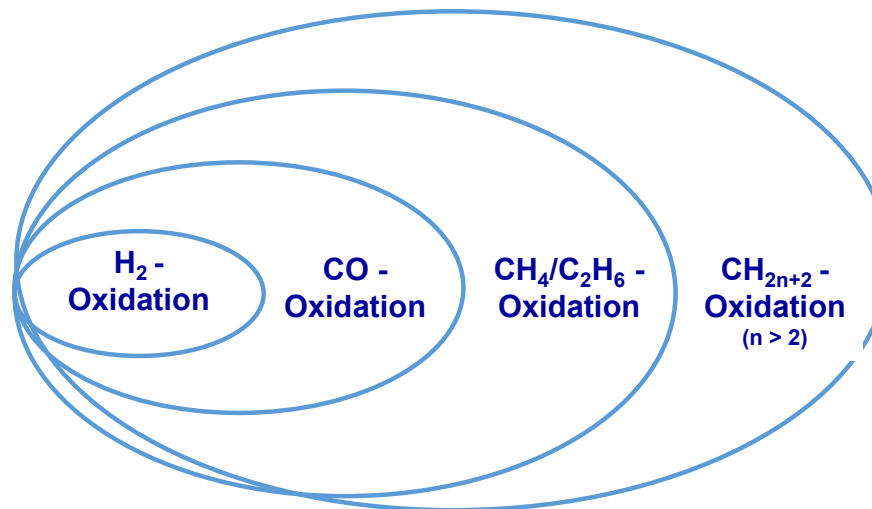
- Viscosity
- Diffusion
- Thermal Conductivity
- Thermal Diffusion
- Speed of Sound

### Thermo-chemical Properties

- Enthalpy, Entropy of formation
- Constant pressure and constant volume heat capacities
- Compressibility
- Thermal Expansion

## Hierarchical Mechanism Structure

- Chemical behavior of small species is almost independent of surrounding species since it is a function of its chemical interaction potential
- This holds as well for the transport properties



Molecule	H <sub>2</sub>	CH <sub>4</sub>	C <sub>3</sub> H <sub>8</sub>	C <sub>6</sub> H <sub>14</sub>	C <sub>16</sub> H <sub>34</sub>
	Hydrogen	Methane	Propane	Hexane	Cetane
Species	9	30	100	450	1200
Reactions	34	200	400	1500	7000



## Reduced Chemical Kinetic Schemes

Detailed schemes are often far too large to be included in 3D-unsteady CFD tools. Hence, reduced schemes are required which are small enough to be included in CFD tools (< 15 species, < 20 reactions) but sufficiently accurate to produce reasonable results.

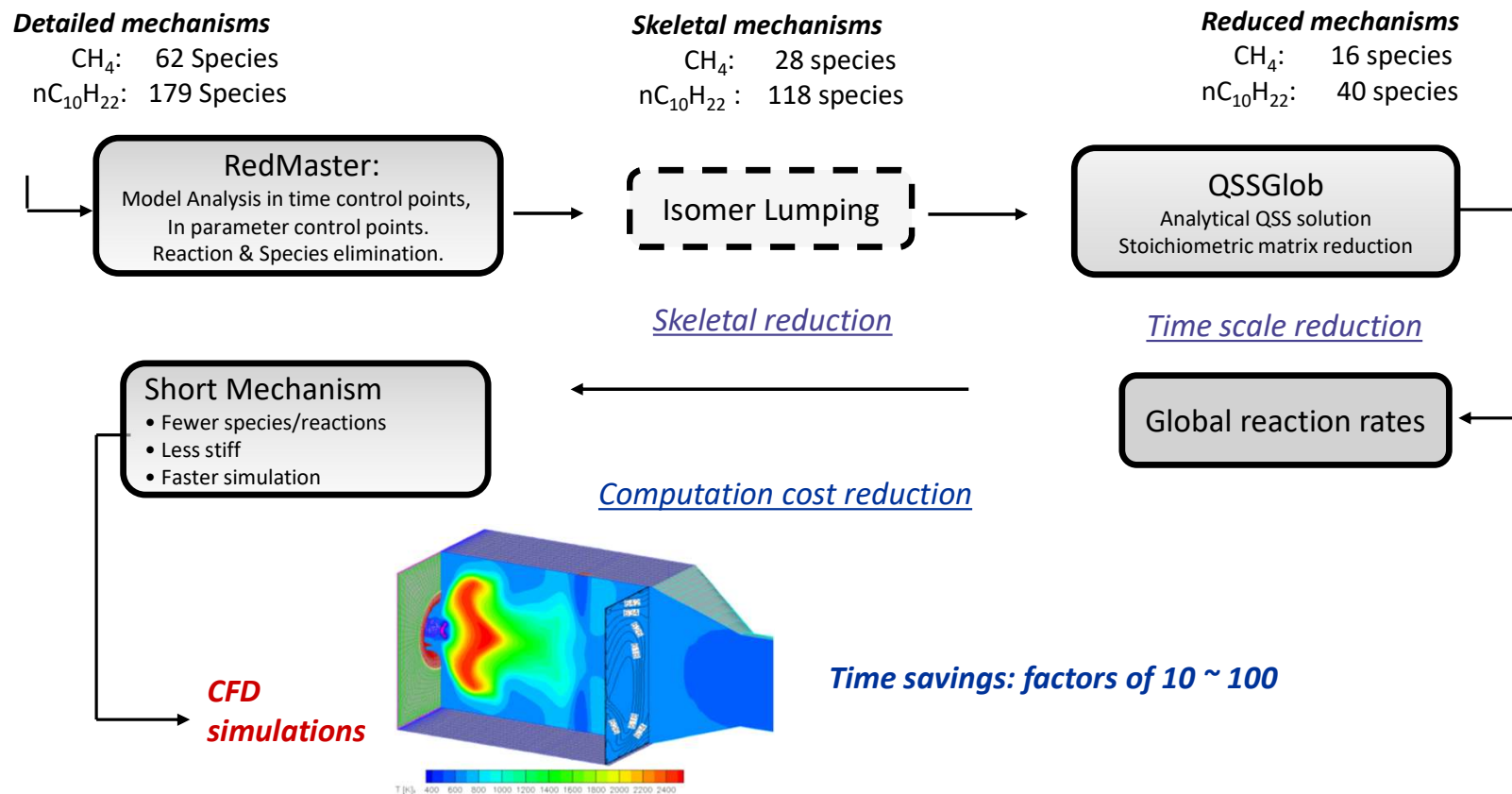
### Different methods to handle this problem

- Flamelet library based models
  - Adiabatic flamelet
  - Non-adiabatic flamelets
  - Flamelet Generated Manifolds (FGM)
- Finite rate chemistry models
  - Chemical based reduction
    - Physico-chemical
    - Flame structure
  - Mathematical based reduction
    - Intrinsic low dimensional manifold (ILDm)
    - Quasi-steady state analysis (QSSA)
    - Computational singular perturbation (CSP)
    - Sensitivity analyses (SA)

(quite often they use detailed kinetic model but assume chemical equilibrium)

(reduced kinetic schemes essential)

## Strategy and Tools for Mechanism Analysis and Reduction

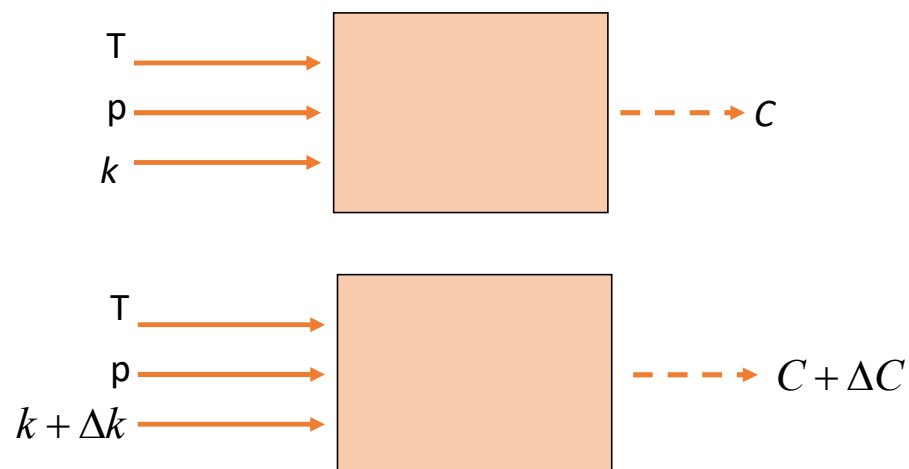


## Mechanism Analysis

### Local Sensitivity Coefficient

Determination of the sensitivity of a solution to a perturbation in vector  $C$  with  $\theta_j$  any perturbation and the result  $\Psi_i$  of the system to the perturbation:

$\theta_j$



$\Psi_i$

$$S = \frac{\Delta C}{\Delta k} \quad \Rightarrow \quad s_{ji} = \frac{\partial c_j}{\partial \theta_i} \quad \text{Sensitivity coefficient}$$



## Mechanism Analysis

### Local Normalized Sensitivity Coefficient

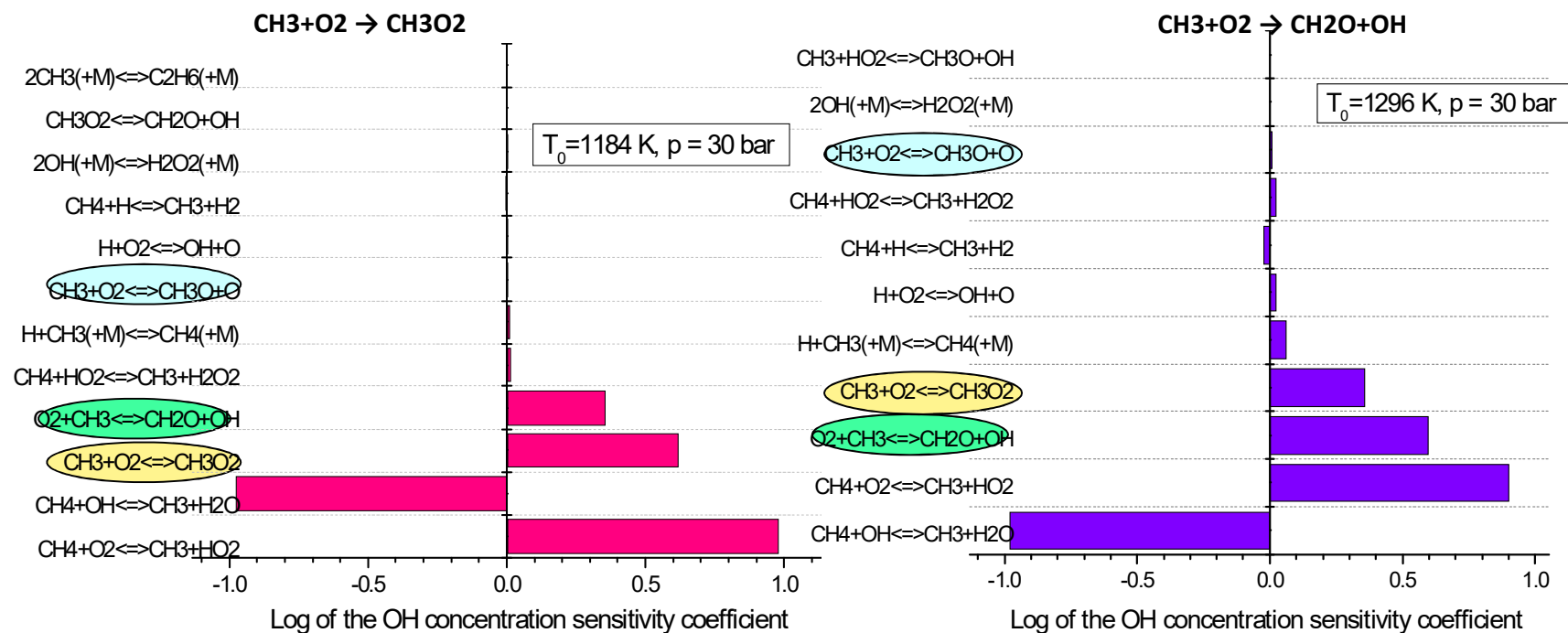
$$S_j = \frac{\theta_j}{\Psi_i} \frac{\partial \Psi_i}{\partial \theta_j} = \frac{\partial \ln \Psi_i}{\partial \ln \theta_j}$$

Overall normalized sensitivity coefficient  $B_i$  is the sum of all local sensitivity coefficient

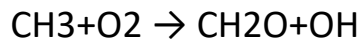
$B_i$  is a measure of the effect of changing parameter  $\theta_i$  on the group of perturbed outputs

$$B_i = \sum_j^p \left( \frac{\partial \ln \Psi_j}{\partial \ln \theta_i} \right)^2$$

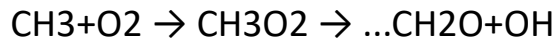
## Sensitivity of Ignition delay (OH concentration) to reaction rates



Two concurrent  
channels:

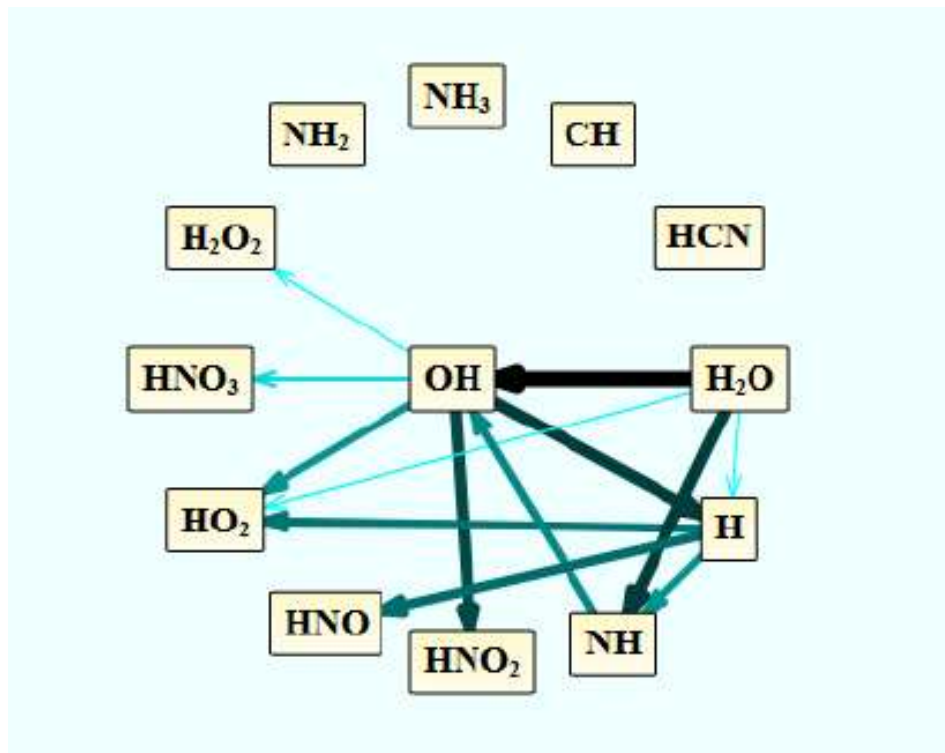


(for  $T > 1200 \text{ K}$ )



(for  $T < 1200 \text{ K}$ )

## Rate of Production Analysis



A calculation of reaction contributions to the production rates of species:

The reaction  $i$  can be considered as unimportant if the rate of production  $R_{ij}$  of species  $j$  in reaction  $i$ , is less than a chosen  $\delta$  for all times in comparison to the maximum of the corresponding rates in all other occurring reactions

$$\Delta R_{ij} = \int_0^{\tau} W_{ij} dt < \delta$$

$$W_{ij} = \frac{v_{ij} w_i}{v_{\max,j} w_{\max}}$$

## Flow of Atoms Analysis

Discrimination of reactions or species on the base of calculation of the flux of atom  $A$  from species to species in each reaction step.

$$\text{Atom flux } A_{ijk} = (w_i n_{A,j} n_{A,k}) / N_{A,i}$$

$n_{A,j}$  is the number of atoms  $A$  in  $j$ ,  $n_{A,k}$  is the number of  $A$  in  $k$ , and  $N_{A,i}$  is the total number of  $A$  in the reaction  $i$ .

$$\xi_{A,k} = (|F_{A,k}^+| - |F_{A,k}^-|) / F_A^{tot}$$

$$F_{A,k}^+ = \sum_{i,j} \{A_{ijk} > 0\} \quad F_{A,k}^- = \sum_{i,j} \{A_{ijk} < 0\}$$

$F_A^{tot}$  the total atomic flux for a given flow chart

$F^+ F^-$  the fluxes for formation and consumption of  $A$ .

A species may be neglected when it is almost stationary  $\xi \rightarrow 0$  and also when its net atomic fluxes  $A$  are small compared to  $F_A^{tot}$ .



## Determination of Important Reactions

The overall sensitivity type measure for identification of important reactions:

$$A_i = \sum_j^K \left( \frac{\partial \ln R_j}{\partial \ln k_i} \right)^2$$

$R_j$  - the rate of production of species  $j$ ,

$k_i$  - coefficient of reaction rate  $i$ ,

$K$  - is a number of species in a model.

A reaction  $i$  is considered important if its coefficients  $A_i$ , calculated as sum for all species are bigger than a chosen threshold

$$A_i \geq \Delta$$

## Determination of Important Species

The overall normalized sensitivity coefficient:

$R_i$  - the rate of production of species  $i$ ,

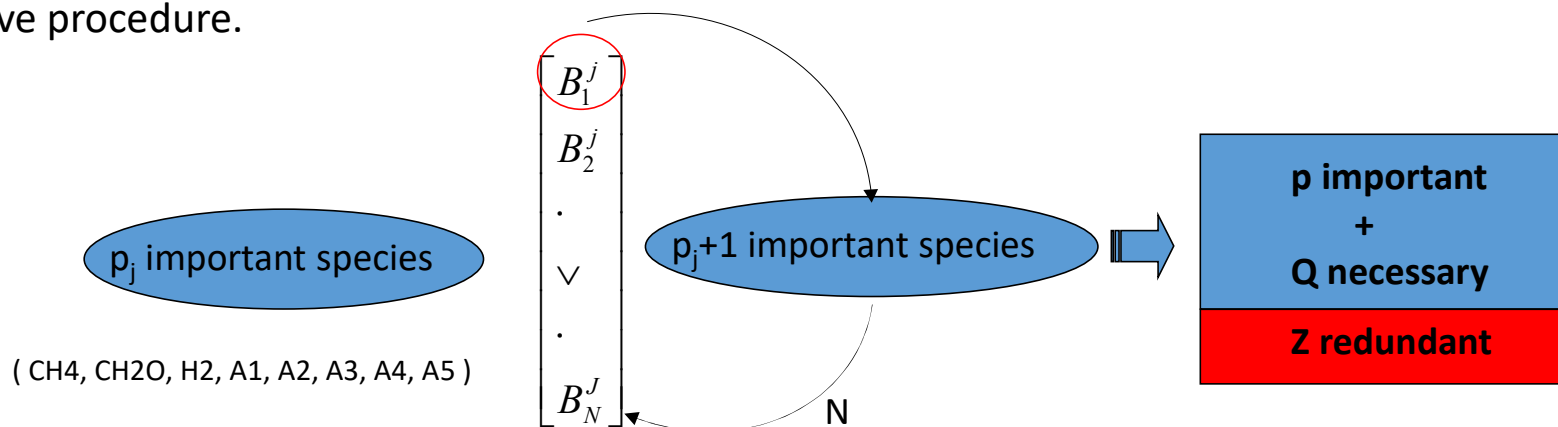
$c_j$  - concentration of species  $j$ ,

$p$  - the number of important species given by the investigator.

$$B_j = \sum_i^p \left( \frac{\partial \ln R_i}{\partial \ln c_j} \right)^2$$

$B_j$  yields the effect of a change of the concentration of species  $c_j$  on the rate of production of species  $i$ ,  $R_i$ , from group of  $p$  important species.

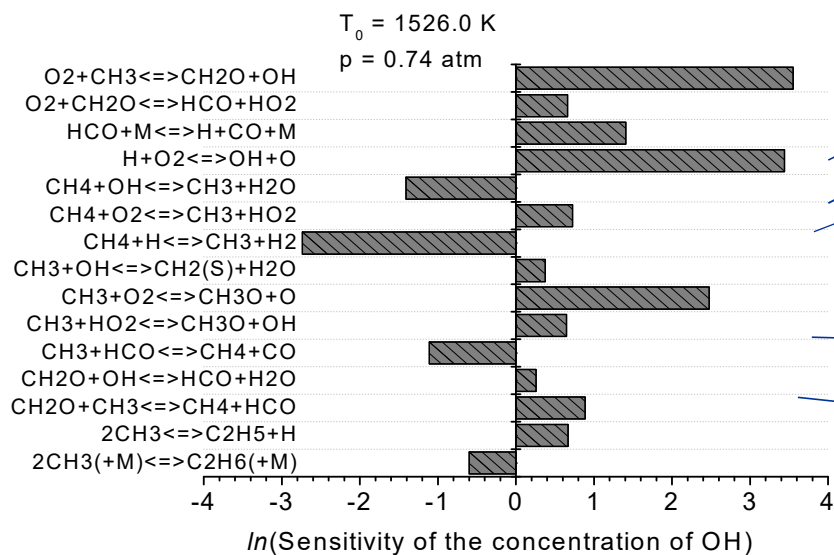
The group of necessary species, which are most coupled with important species has to be identified by an iterative procedure.



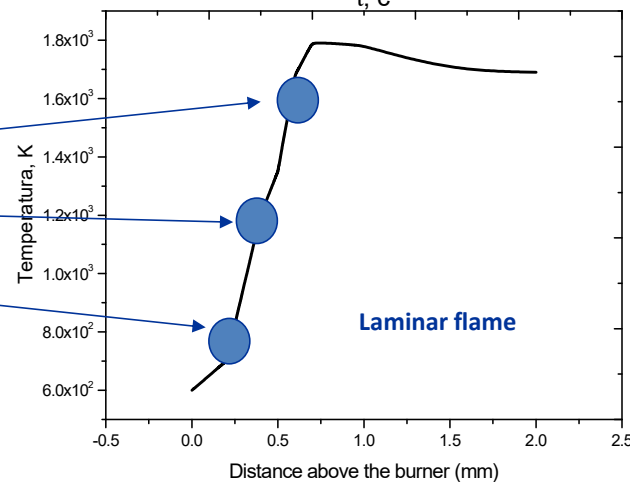
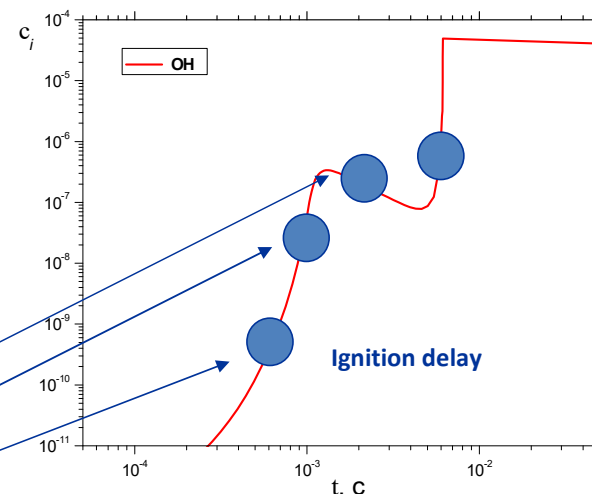
## Multi-target Global Sensitivity Analysis

RedMaster Code:  
 Reaction & Species elimination with  
 Multi target Sensitivity Analysis  
 in time control points

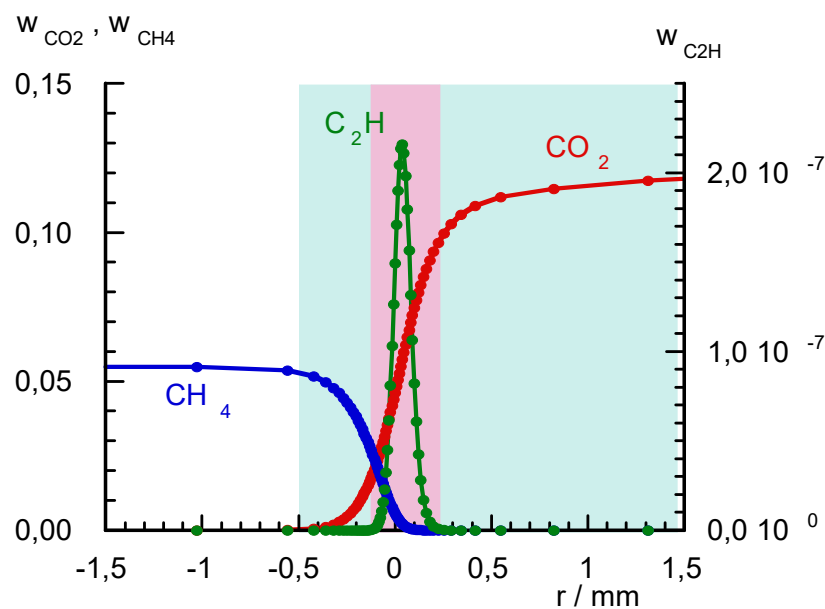
$$S = \frac{\Delta C}{\Delta k}$$



Slavinskaya, Haidn, AIAA 2008-1012, 2008



## Time Scale Methods: QSS Approach

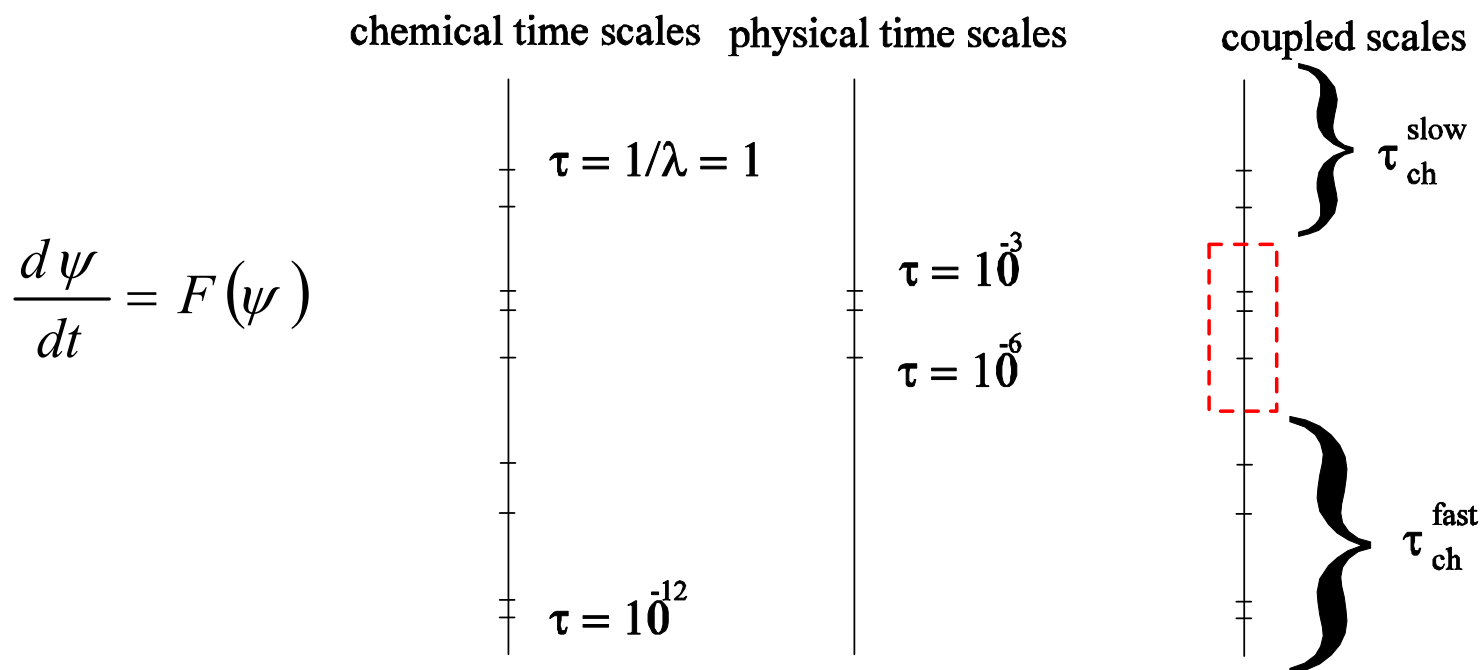


1-dimensional cut through a CH<sub>4</sub>-air flame

### Problems:

- extremely high dimensionality of the system!
  - non-linear chemical source terms
  - stiffness of the governing equation system
  - different chemical time scales do not only introduce stiffness, but also cause the existence of very small length scales
- **Is it possible to decouple the fast chemical processes?**
- This would
    - reduce the number of governing equations
    - remove part of the scaling problems in space!

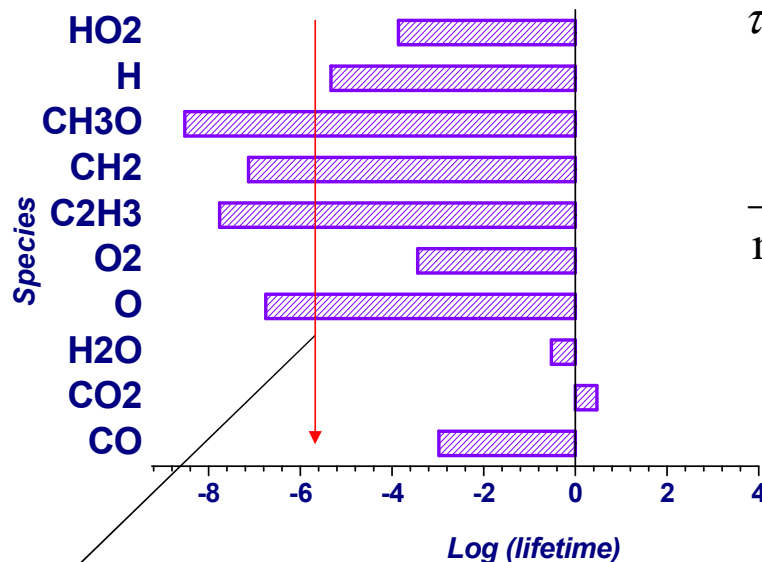
## Multi – Scales and Hierarchy of Processes



Chemical kinetic ODEs are multi-scale models: processes with different time scales – STIFF ODEs

## Time Scale Methods: QSS Species

- the rate at which species  $i$  is consumed is much faster than the rate by which it is produced
- the concentrations and lifetime of QSS species are very small



QSS species: CH3O, O, CH2, C2H3

$$\tau_i^c = -1 / \frac{\partial \omega_i}{\partial c_i} = |1 / J_{ii}|$$

$$\frac{|R_j^p - R_j^c|}{\max(|R_j^p|, |R_j^c|)} \ll \delta$$



$$\frac{dC_{QSSj}}{dt} = 0$$

Searching for the Quasi-Steady-State (QSS) species (mostly intermediate radicals) to obtain more simple system of kinetic equations .

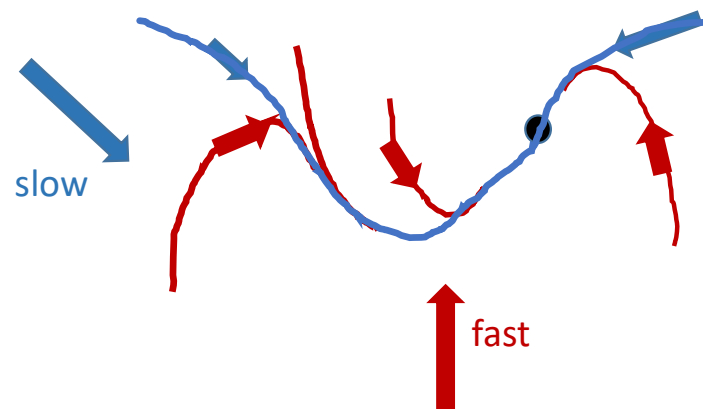
## Intrinsic Low Dimensional Manifold

Slow chemical processes solved with the flow

- Decouple fast and slow chemical processes.
- Reduce number of equations
- Fast time scales are determined from slow ones

Identify Intrinsic Low-Dimensional Manifolds (ILDM).

- Reduce kinetics to the manifolds.
- Project governing equations onto the manifold.



## Reduction of Reaction Mechanisms

Detailed reaction mechanism

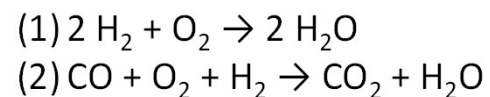
Skeletal reaction mechanism  
 reduction factor 2-5)

- 1)  $O + H_2 \rightarrow H + OH$
- 2)  $H + OH \rightarrow O + H_2$
- 3)  $O + HO_2 \rightarrow OH + O_2$
- 4)  $H + O_2 + M \rightarrow HO_2 + M$
- 5)  $H + O \rightarrow O + H$
- 6)  $O + OH \rightarrow H + O_2$
- 7)  $H + OH + M \rightarrow H_2O + M$
- 8)  $H + HO_2 \rightarrow O + H_2O$
- 9)  $H + HO_2 \rightarrow O_2 + H_2$
- 10)  $OH + H_2 \rightarrow H + H_2O$
- 11)  $2OH \rightarrow O + H_2O$
- 12)  $OH + CO \rightarrow H + CO$
- 13)  $O + H_2O \rightarrow 2OH$
- 14)  $H + CO \rightarrow OH + CO$
- 15)  $H + HO_2 \rightarrow 2OH$
- 16)  $HCO + M \rightarrow H + CO + M$
- 17)  $H + CO + M \rightarrow HCO + M$
- 18)  $H + HCO \rightarrow H_2 + CO$
- 19)  $HCO + O \rightarrow HO_2 + CO$

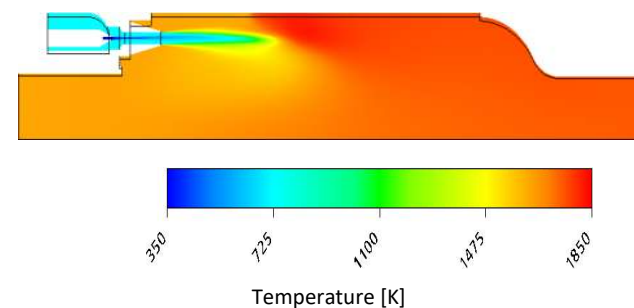
RedMaster Code:  
 Multi target analysis and  
 Reduction with keeping  
 of predictive capabilities

QSSGlob Code  
 Analytical QSS solution  
 Stoichiometric matrix reduction

Global reduced mechanism (reduction factor 2 - 3)



Numerical simulation





## Reduced Mechanism Validation

Validation has to happen already during development

In order to be highly predictive it is mandatory to

- Use the largest possible data base with parameter variations of
  - Pressure
  - Initial temperature
  - Mixture ratio
  - Diluent concentrations

and is also recommended to take data from a sufficient large number of different experimental setups using as well different measurement techniques.

However, never forget to check the published data about uncertainty to avoid being led astray (i.e. old data from rapid compression engines can be biased due to induced convection, shock tubes should have a sufficient large diameter to reduce boundary layer effects, ....)



## Final Mechanism Validation Ignition Delay

Ignition delay times at low pressure are important for modeling the engine ignition and startup process but as well at higher pressures and different mixture ratios.

Furthermore, laminar flame speed is of key importance since it can be measured rather easily and it is defined by the heat release, i.e., the progress of the chemical reactions. Again, it is important to validate against for low pressure and high pressure data at various mixture ratios.

There are reactions which react differently depending on pressure ( intermolecular collisions are responsible for this behavior).



# What you should remember



- Explosive limits of H<sub>2</sub>/O<sub>2</sub> mixtures
- General reaction mechanism (initiation, propagation and termination)
- Difference between light hydrocarbon (methane) and heavy hydrocarbon reactions
- NTC region for higher alkane combustion and its explanation
- Methods to generate reduced chemical kinetic schemes
- Development and validation procedures of such schemes



## Mechanism for Ammonium-perchlorate Decomposition

		Arrhenius parameters		
		A	b	Ea
1)	$\text{HClO}_4 \rightleftharpoons \text{ClO}_3^* + \text{OH}^*$	1.0 e14	0.0	39100
2)	$\text{HClO}_4 + \text{HNO} \rightleftharpoons \text{ClO}_3^* + \text{H}_2\text{O} + \text{NO}^*$	1.5 e13	0.0	6000
3)	$\text{ClO}_3^* \rightleftharpoons \text{ClO}^* + \text{O}_2$	1.7 e13	0.5	0.0
4)	$\text{Cl}_2 + \text{O}_2 + \text{M} \rightleftharpoons \text{ClO}_2^* + \text{Cl}^* + \text{M}^*$	6.0 e08	0.0	1200
5)	$\text{ClO}^* + \text{NO}^* \rightleftharpoons \text{Cl}^* + \text{NO}_2^*$	6.78 e12	0.0	311
6)	$\text{ClO}^* + \text{ClOH} \rightleftharpoons \text{Cl}_2 + \text{HO}_2^*$	1.0 e11	0.0	10000
7)	$\text{ClOH} + \text{OH}^* \rightleftharpoons \text{ClO}^* + \text{H}_2\text{O}$	1.8 e13	0.0	0
8)	$\text{HCl} + \text{OH}^* \rightleftharpoons \text{Cl}^* + \text{H}_2\text{O}$	5.0 e11	0.0	750
9)	$\text{Cl}_2 + \text{H}^* \rightleftharpoons \text{HCl} + \text{Cl}^*$	8.4 e13	0.0	1150
10)	$\text{ClO}^* + \text{NH}_3 \rightleftharpoons \text{ClOH} + \text{NH}_2^*$	6.0 e11	0.5	6400
11)	$\text{NH}_3 + \text{Cl}^* \rightleftharpoons \text{NH}_2^* + \text{HCl}$	4.5 e11	0.5	100
12)	$\text{NH}_3 + \text{OH}^* \rightleftharpoons \text{NH}_2^* + \text{H}_2\text{O}$	5.0 e07	1.6	955
13)	$\text{NH}_2^* + \text{O}_2 \rightleftharpoons \text{HNO} + \text{OH}^*$	3.0 e09	0.0	0
14)	$\text{NH}_2^* + \text{NO}^* \rightleftharpoons \text{H}_2\text{O} + \text{N}_2$	6.2 e15	-1.3	0
15)	$\text{HNO} + \text{OH}^* \rightleftharpoons \text{NO}^* + \text{H}_2\text{O}$	1.3 e07	1.9	-950
16)	$\text{HNO} + \text{O}_2 \rightleftharpoons \text{NO}_2^* + \text{OH}^*$	1.5 e13	0.0	10000
17)	$\text{HNO} + \text{H}^* \rightleftharpoons \text{H}_2 + \text{NO}^*$	4.5 e11	0.7	660
18)	$\text{NO}^* + \text{H}^* + \text{M} \rightleftharpoons \text{HNO} + \text{M}$	8.9 e19	-1.3	740
19)	$\text{HO}_2^* + \text{N}_2 \rightleftharpoons \text{HNO} + \text{OH}^*$	2.7 e10	0.5	41800
20)	$\text{NO}^* + \text{HO}_2^* \rightleftharpoons \text{NO}_2^* + \text{OH}^*$	2.11 e12	0.0	480
21)	$\text{H}^* + \text{NO}_2^* \rightleftharpoons \text{NO}^* + \text{OH}^*$	3.47 e14	0.0	1480
22)	$\text{H}_2 + \text{OH}^* \rightleftharpoons \text{H}_2\text{O} + \text{H}^*$	2.16 e08	1.5	3430

$$k = AT^b e^{-Ea/T}$$



## Mechanism for Ammonium-perchlorate / HTPB Reactions

